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## PURIFICATION OF MINERALIZED WATERS FROM U(VI) COMPOUNDS USING BENTONITE/IRON OXIDE COMPOSITES

Об'єктом дослідження є бентонітові глини, основним породоутворюючим мінералом яких є монтморилоніт. Даний природний силікат проявляє сорбційну здатність до іонів важких металів завдяки високій катіонообмінній ємності та питомій поверхні. Одним з найбільш проблемних місць використання монтморилоніту в сорбційних процесах є здатність до набухання у водних середовищах. Це значно ускладнює відділення відпрацьованого сорбенту від очищеної води. Для усунення даного недоліку найчастіше використовують гранулювання з подальшою термічною обробкою. При цьому в якості структуроутворюючого агенту застосовують різні полімерні сполуки. Такий прийом призводить до значного зменшення питомої поверхні бентонітових глин, а значить, і погіршення їх сорбційних властивостей. В ході дослідження використовували метод модифікування поверхні монтморилоніту оксигідроксидами феруму (феригідритом). Отримані матеріали відрізняються технологічністю та підвищеною сорбційною здатністю по відношенню до сполук урану. Це пов'язано з тим, що при обробці поверхні бентонітових глин феригідритом можна отримати ефективні сорбенти, які втрачають здатність до набухання без термічної обробки. Нанесення шару ферумоксидних сполук на поверхню монтморилоніту привело до зміни параметрів поруватої структури отриманого композиту. Так, питома поверхня модифікованого зразку становить 250 м<sup>2</sup>/г, що значно перевищує таку для вихідного мінералу (89 м²/г). При цьому у 2,8 рази збільшився середній розмір пор. Показано, що внаслідок обробки поверхні монтморилоніту феригідритом відбувається зростання сорбційної здатності матеріалів щодо сполук урану зі збільшенням вмісту заліза на поверхні: від 0,42 мг/г для вихідного монтморилоніту до 10,13 мг/г для модифікованого зразку. Встановлено, що присутність конкирентних металів (As, Mn, Co, Cd, Cr) в мінералізованих водах в еквімолярних кількостях не призводить до суттєвої зміни величин адсорбції урану на бентоніт/ферумоксидних композитах.

Ключові слова: очищення води, сорбція урану(VI), бентоніт, монтморилоніт, оксигідроксиди заліза, мінералізовані води, важкі метали.

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## **1.** Introduction

The development of the uranium mining and uranium processing industries causes significant environmental pollution, in particular the water basin. Underground or aggregate leaching of uranium, the presence of waste storage facilities for hydrometallurgical processing of uranium ores lead to the entry into the groundwater and groundwater compounds of uranium and other heavy metals and radionuclides [1, 2].

The increased content of heavy metals and radionuclides in water poses a threat to human health [2, 3]. Uranium compounds are radioactive and quite chemically toxic, the accumulation of uranium in the kidneys leads to irreversible damage and poses a potential risk to life. According to world standards and the World Health Organization (WHO) classification, uranium is a carcinogenic element. The level of its concentration in water should not exceed 30  $\mu$ g/dm<sup>3</sup> according to WHO recommendations [4], 30  $\mu$ g/dm<sup>3</sup> in accordance with the standards of the US Environmental Protection Agency [5] and 40  $\mu$ g/dm<sup>3</sup> in accordance with the State Standards of Ukraine [6].

Uranium in a natural aqueous medium is dissolved in a hexavalent state both in positively charged forms of the uranyl cation  $UO_2^{2^+}$  and in the form of hydroxyl complexes, for example, UO<sub>2</sub>OH<sup>+</sup>, and in neutral UO<sub>2</sub>(OH)<sub>2</sub>, UO<sub>2</sub>CO<sub>3</sub> and negatively charged forms (UO<sub>2</sub>)<sub>2</sub>CO<sub>3</sub>(OH)<sub>3</sub>. In the tetravalent state, uranium is much less soluble [7, 8]. As a result of the use of acid leaching in hydrometallurgical processes, in addition to the high content of U(VI) compounds, groundwater in places of uranium ore mining and processing is characterized by increased mineralization, which amounts to several grams per liter [9]. In such waters, U(VI) is predominantly in the form of negatively charged sulfate or carbonate complexes [10], while the solubility of uranium in mineralized waters increases [8]. Heavy metals and radionuclides, which are also present in contaminated mineralized waters [11], mutually affect the solubility of uranium and each other.

The removal of heavy metals and uranium from wastewater is carried out using reagent methods, membrane separation methods and their combination: deposition, oxidation, coagulation, ultrafiltration, reverse osmosis, etc. However, only the sorption method ensures the removal of uranium and heavy metals from polluted waters to the very low levels that can't be achieved using other methods.

Various materials are used to remove uranium, such as activated carbon, synthetic resins, zeolites, materials of biological origin, etc. Synthetic sorption materials have a high efficiency of removing inorganic toxicants, but their disadvantage is their high cost and multi-stage synthesis. The use of clays as sorbents is promising given the various possibilities of modifying their surface to create functional materials with new improved properties. Surface treatment of clay minerals with iron oxides and hydroxides increases their adsorption capacity with respect to inorganic toxicants [12, 13]. Moreover, the obtained sorbents have both anion-exchange and cation-exchange properties.

Therefore, the development of composites based on natural clay minerals by modifying them with iron compounds for the effective extraction of uranium compounds and other inorganic toxicants from contaminated mineralized waters is a timely and relevant task, and is the subject of this research.

# 2. The object of research and its technological audit

The object of research is bentonite clays, the main mineral of which is montmorillonite – a clay mineral with a layered structure. Montmorillonite forms a 2:1 type structure with two tetrahedral and octahedral layers between them, its structural formula is  $Al_3Mg[Si_4O_{10}](OH)_2 \cdot nH_2O$  [14]. Water molecules located in the interlayer space of montmorillonite lead to the lid of structural packets. The active Al(Si)OH groups are located mainly on the lateral faces of montmorillonite and are the main factors contributing to the sorption of heavy metal cations and radionuclides.

A technological audit shows that natural clays, and in particular, bentonite, are widely used as sorbents in technological processes of water purification from inorganic toxicants found in cationic forms in waters. The surface of clay particles is predominantly negatively charged and therefore heavy metals and radionuclides that are in anionic form are not adsorbed on it. The sorption properties of clay minerals can be significantly improved by modifying their surface. Therefore, silicates, the surface of which is modified with various organic and inorganic compounds, are very promising for the removal of trace amounts of heavy metals and radionuclides from contaminated aqueous media.

#### 3. The aim and objectives of research

*The aim of research* is to obtain bentonite/iron oxide composites for the extraction of uranium and heavy metals from polluted waters. Research objectives:

1. Synthesize bentonite/iron oxide composites and study their physicochemical characteristics.

2. To study the features of the sorption purification of contaminated mineralized waters from uranium and heavy metals by synthesized bentonite/iron oxide compounds.

### 4. Research of existing solutions of the problem

The removal of uranium compounds from polluted waters is carried out by various methods. One of them is chemical precipitation, oxidation, and coagulation methods that require the use of chemical reagents [15, 16]. Membrane separation methods are also widely used, including ultrafiltration, nanofiltration, and reverse osmosis [17, 18]. However, sorption technologies are the most effective in treating water from heavy metals. To date, a large number of sorbents of various nature and origin, in particular synthetic materials, are developed [19, 20]. Sorbents based on zeolites and natural clay minerals are also obtained [21, 22]. Biosorbents are actively developed, for which algae and microorganisms are the raw material [23, 24]. Particular attention in the literature is given to studying the latest sorption materials for the extraction of inorganic toxicants [25, 26] primarily because only through sorption methods can high levels of purification of polluted waters is achieved.

The prospects of using sorbents based on iron and its compounds for the extraction of uranium and heavy metals from polluted waters are described in a significant number of works. The use of micro- and nanoscale iron in the processes of sorption extraction of uranium is studied [27, 28]. The effectiveness of water purification from natural radionuclides on iron oxides is also studied [29, 30]. Significant sorption ability with respect to uranium compounds is exhibited by (oxy) iron hydroxides (III) [31, 32]. High sorption properties of iron compounds indicate the possibility of creating the latest sorption materials based on them. Ferric oxides (for example, ferrihydrite, goethite and hematite) effectively remove uranium (VI) compounds and heavy metals from water in a neutral medium [13]. However, the drawback of such sorbents is the ability to aggregate particles during synthesis [33, 34]. The application of the reaction layer of ferrum compounds to special substrates (clay minerals, activated carbon, ion-exchange resins, etc.) makes it possible to increase the aggregative stability of materials [31]. Thus, the sorbents obtained by depositing iron oxides and hydroxides on the surface of clay minerals have enhanced sorption properties for uranium and heavy metals due to the cation exchange ability of clay minerals and the anion exchange properties of supported iron compounds.

Thus, the development of bentonite/iron oxide composites will make it possible to obtain material based on cheap natural raw materials with improved structural and sorption characteristics. The study of the conditions for the effective extraction of uranium from contaminated waters on bentonite modified with iron compounds is carried out taking into account the peculiarities of sorption of uranium in mineralized waters, the presence of arsenic, manganese, cobalt, cadmium, chromium compounds in the solution.

### 5. Methods of research

The synthesis of bentonite/iron oxide composites was carried out by treating the surface of montmorillonite (MMT) with iron salts (III) according to a modified procedure [35]. To do this, in a 0.2 M solution of Fe(NO<sub>3</sub>)<sub>3</sub>·9H<sub>2</sub>O, a weighed silicate was introduced in various mass ratios of Fe(g): clay mineral (g) – 0.01:1; 0.05:1; 0.1:1 and 1:1 to obtain samples of bentonite/iron oxide composites Fh-MMT 0.01-1; Fh-MMT 0.05-1; Fh-MMT 0.1-1; Fh-MMT 1-1. The suspension was stirred for 1 h, after which a 1 M KOH solution was added to pH 7–8. The resulting precipitate was washed with distilled water from excess salts, sedimented and filtered under vacuum. The resulting samples were dried at 80 °C in an oven, triturated and sieved to obtain a fraction of  $\leq 0.2$  mm. Samples were stored in containers without air.

The structure of the initial and modified samples was studied by diffraction (X-ray phase analysis (XRD)) using oriented preparations using a DRON-4-07 diffractometer manufactured by the USSR (2–60°  $2\theta$ , CuK $\alpha$  radiation).

To determine the parameters of the porous structure of montmorillonite and iron oxide composites, the method of low-temperature nitrogen adsorption-desorption (Quantachrome Nova 2200e Surface Area and Pore Size Analyzer, United States) was used. Samples were evacuated at room temperature for 30 minutes and kept for 5 minutes after equilibrium is established at each point of the isotherm. The specific surface area and total pore volume were determined by the Brunauer, Emmett, and Teller (BET) methods, and the pore size distribution was determined by the Barrett-Joyner-Halenda (BJH) method [36].

The size of aggregates in clay samples and the  $\zeta$  potential were determined using the Zetasizer Nano ZS Malvern Instrument (United Kingdom) according to the Henry equation using the Oshima approximation [37, 38].

Water purification from pollution by uranium (VI) compounds using bentonite/iron oxide composites was studied in a wide range of concentrations. To prepare aqueous solutions of uranium (VI), the uranyl sulfate salt  $UO_2SO_4$ ·3H<sub>2</sub>O (concentration  $10^{-2}$  M) was used.

The study of the processes of sorption purification of contaminated water was carried out using solutions whose composition according to the main anionic components corresponded to the composition of underground saline water at the liquid waste storage facility for processing uranium ores of the Eastern Mining and Processing Combine (Zhovti Vody, Ukraine):  $HCO_3^- - 450$ ,  $Cl^- - 180$ ,  $SO_4^{2-} - 2830$ ,  $NO_3^- - 130 \text{ mg/dm}^3$  [9]. The output solutions were prepared on the basis of the corresponding sodium salts, the total salt content was 5200 mg/dm<sup>3</sup>, pH 7.2. The pH value of water systems was adjusted with 0.1 M NaOH solution and monitored with a pH-meter pH-150M (Republic of Belarus).

Sorption extraction of uranium (VI) bentonite/iron oxide composites was carried out under static conditions at room temperature. The volume of the aqueous phase was 50 cm<sup>3</sup>, the weighed portion of the sorbent was 0.1 g. To establish adsorption equilibrium, the samples were continuously shaken for 1 h. The solid and liquid phases were separated by centrifugation (6000 rpm). The uranium (VI) content in the solutions after sorption was determined spectrophotometrically using a UNICO-UV 2100 spectrophotometer (USA) using an Arsenazo III reagent at a wavelength of 665 nm.

The value of the sorption of uranium (VI) a (mg/g) was calculated by the formula:

$$a = (C_{init} - C_{eq}) \cdot V/m$$
,

where  $C_{init}$ ,  $C_{eq}$  – initial and equilibrium metal concentration, mg/dm<sup>3</sup>; V – volume of the solution, dm<sup>3</sup>; m – mass of the sorbent sample, g.

The experimental isotherms of sorption of uranium (VI) were processed using the Langmuir mathematical model for a homogeneous surface [39]:

$$C_{eq}/a_{eq}=1/(K_L \cdot a_m)+(1/a_m) \cdot C_{eq},$$

where  $a_{eq}$  – equilibrium sorption, mg/g;  $K_L$  – Langmuir constant, characterizing the energy of sorption, dm<sup>3</sup>/mg;  $C_{eq}$  – equilibrium concentration, mg/dm<sup>3</sup>;  $a_m$  – sorption capacity of the monolayer, mg/h.

And also Freundlich models for a heterogeneous surface [40]:

$$\lg a_{eq} = \lg K_F + (1/n) \cdot \lg C_{eq},$$

where  $K_F$  – Freundlich constant characterizing the sorption capacity, dm<sup>3</sup>/h; 1/*n* – Freundlich constant, which characterizes the intensity of sorption.

The distribution of the forms of the presence of U(VI), Cd(II), Co(II), Cr(VI), Mn(II), As(V) cations in solution was calculated using the Medusa software [41].

Sorption of uranium (VI) extraction is iron oxide composites from mineralized waters in the presence of other cations Cd(II), Co(II), Cr(VI), Mn(II), As(V) were studied under conditions of their equimolar content in solution (ratio of uranium (VI)/Me 1:1) at a concentration of  $10^{-4}$  M, pH 7.2, mineralization 5.2 g/dm<sup>3</sup>. Aqueous solutions of heavy metal salts were prepared using the corresponding salts Na<sub>2</sub>HAsO<sub>4</sub>·7H<sub>2</sub>O, CoCl<sub>2</sub>·6H<sub>2</sub>O, K<sub>2</sub>Cr<sub>2</sub>O<sub>7</sub>, MnCl<sub>2</sub>·4H<sub>2</sub>O, Cd(NO<sub>3</sub>)<sub>2</sub>·4H<sub>2</sub>O (concentration  $10^{-2}$  M). The equilibrium concentration of each metal in solution was determined by inductively coupled plasma atomic absorption spectrometry (Thermo Scientific iCAP 7400 ICP-OES, USA).

The degree of water purification (%) from U(VI), Cd(II), Co(II), Cr(VI), Mn(II), As(V) was calculated by the formula:

$$CO = (C_{init} - C_{eq})/C_{init} \cdot 100,$$

where  $C_{init}$ ,  $C_{eq}$  – initial and equilibrium metal concentration, mg/dm<sup>3</sup>.

### **6**. Research results

Fig. 1 shows the diffraction patterns of iron oxide composites (Fh-MMT) with different ratios of ferrihydrite and output bentonite (MMT).



**Fig. 1.** Diffraction patterns of 1 – initial (MMT) and 2, 3 – modified bentonite: 2 – (Fh-MMT 0.05-1), 3 – (Fh-MMT 1-1)

The bentonite diffraction pattern shows an intense basal reflection  $d_{001}=1.26$  nm, which is typical for air-dried samples of the main mineral of bentonite clays – montmorillonite [42]. The diffraction patterns of Fh-MMT 0.05-1 (curve 2) are very similar to those for MMT, but the  $d_{001}$ reflection is less intense, which suggests that some of the added Fe(III) is located in the interlayer space of montmorillonite [43]. The practical X-ray amorphism of the Fh-MMT 1-1 sample can be explained by the presence of ferric iron in the interlayer space of montmorillonite. It can also be explained by the formation of ferrihydrite on the surface of montmorillonite in the form of thin films or very small clusters, or particles (iron oxide/nanoparticle co-aggregates), which, according to existing literature data [44], have an average size of 6 nm.

As can be seen from Fig. 2, the nature of the nitrogen adsorption – desorption isotherm on the starting montmorillonite is typical of microporous sorbents, the hysteresis loop is weakly expressed, and according to the Brunauer, Emmett, and Teller (BET) classification, it belongs to the first type of isotherms [45].

For modified montmorillonite samples, the shape of the hysteresis loops in accordance with the recommendations of IUPAC (International Union of Pure and Applied Chemistry) is of H2 type, which is characterized by slitshaped pores with flat parallel walls.



Fig. 2. Nitrogen sorption-desorption isotherms on the initial (MMT) and modified bentonite (Fh-MMT 0.05-1), (Fh-MMT 1-1)

Table 1 shows the parameters of the porous structure of the samples (specific surface area *S*,  $m^2/g$ , total pore volume  $V_{\Sigma}$ , cm<sup>3</sup>/h, micropore volume  $V_{\mu}$ , cm<sup>3</sup>/g and pore size distribution  $r_1$ ,  $r_2$ , nm).

An analysis of the parameters of the porous structure according to the results of low-temperature adsorption-desorption of nitrogen at 77 K of bentonite/iron oxide composite materials indicates that, during the deposition of ferrihydrite on the surface of silicate, the total specific surface of the obtained sorbent increases to 250 m<sup>2</sup>/g. This is 2.8 times higher than the total specific surface area for a natural mineral, while the pore volume also increases by 2.8 times.

Fig. 3 shows the character of the dependence of the  $\zeta$  potential on the pH of the medium obtained by measuring the electrokinetic parameters of the particles in the dispersions of the output and bentonite modified with ferrihydrite.

The  $\zeta$  potential for the initial sample in the entire pH range is negative and amounts to (-20)-(-70) mV. This is due to the developed double electric layer (DEL) of exchange cations at negatively charged basal surfaces of planar mineral particles [46]. The pH dependence of the  $\zeta$  potential for samples modified by ferrihydrite repeats that for the initial samples, but the  $\zeta$  potential increases by 30–40 mV over the entire pH range and amounts to (7)-(-38) mV.



Fig. 3. The dependence of the zeta potential of the output (MMT) and modified samples (Fh-MMT 1-1) on pH

The values of the hydrodynamic diameter of the particles in the solution are given in Table 2. The data presented indicate a significant polydispersity of systems. In the output samples, particles with a diameter of ~570 nm and ~4900 nm, with a predominance of small particles, predominate. Clay modification with ferrihydrite leads to an increase in particle size to ~1600 nm and ~5000 nm.

#### Table 2

The value of the hydrodynamic particle diameter (d) obtained by the distribution of particle size by intensity according to dynamic light scattering and the polydispersity coefficient (PdI) in solution

Sample	d, nm	Pd $I$
MMT	(57±2)·10 <sup>1</sup> , (49±3)·10 <sup>2</sup>	0.36±0.02
Fh	(14±2)·10 <sup>2</sup> , (53±2)·10 <sup>2</sup>	0.51±0.09
Fh-MMT	$(16\pm 2)\cdot 10^2$ , $(50\pm 4)\cdot 10^2$	0.41±0.06

Fig. 4 shows the sorption isotherms of uranium (VI) bentonite/iron oxide composites and the output sample at pH 7.2 from mineralized waters. The data obtained indicate that, upon modifying the surface of montmorillonite iron oxide-hydroxides, the sorption ability of the obtained samples with respect to uranium (VI) increases in the series MMT

It is known that for clay minerals, in particular montmorillonite, which are cation exchangers, sorption extraction occurs due to the binding of ions  $UO_2^{2+}$  mainly in the active centers of the side faces (aluminol = Al-OH, silanol = Si-OH or bridging groups = Al-OH-Si=). The negative charge of the surface of montmorillonite prevents the adsorption of negatively charged anionic forms of metals on this

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		1		1		
					Pore size distribution, nm	
Sample	<i>S</i> , m²/g	$V_{\Sigma}$ , cm <sup>3</sup> /g	$V_{\mu}$ , cm $^3$ /g	V <sub>µ%</sub> , %	BJH d	V(r)
					Г1	r <sub>2</sub>
MMT	89	0.081	0.016	19.80	1.41	-
Fh-MMT 0.05-1	128	0.141	0.048	34.04	1.54	1.92
Fh-MMT 1-1	250	0.224	0.095	42.41	1.70	1.72

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surface. For modified samples, even with a low content of iron compounds on the surface, there is an increase in the values of sorption extraction of uranium. Such high values of uranium sorption for samples Fh-MMT 0.1-1 and Fh-MMT 1-1 can be explained by the presence of ferric iron in the interlayer space of montmorillonite and the formation of ferrihydrite on the surface of montmorillonite, which leads to the formation of active centers capable of anion exchange = Fe–OH [43].



Fig. 4. The sorption isotherm of U(VI) from mineralized water at 1 – output (MMT) and 2–5 – modified samples: 2 – (Fh-MMT 0.01-1), 3 – (Fh-MMT 0.05-1), 4 – (Fh-MMT 0.1-1), 5 – (Fh-MMT 1-1)

Sorption isotherms were analyzed using the Langmuir and Freindlich equations and the calculation results for the corresponding coefficients are given in Table 3.

The obtained isotherms are described by the Langmuir monomolecular sorption equation for a homogeneous surface (correlation coefficients  $R^2=0.9386\pm0.976$ ) and the empirical Freindlich equation of sorption on a heterogeneous surface, (correlation coefficients  $R^2=0.941\pm0.9915$ ). The maximum sorption values  $A_{\text{max}}$  of uranium (VI) compounds from mineralized waters are observed for samples with a high degree of surface coating with ferrihydrite (Fh-MMT 1-1), these values are 10.13 mg/g, while for the output montmorillonite they are 0.42 mg/g.

The sorption extraction of heavy metals and, in particular, uranium from aqueous solutions is significantly affected by the presence of ion-borne forms of metals in these solutions. Using the Medusa program, it was determined that for uranium in waters with high salinity, the main forms in the acidic region are sulfate complexes  $UO_2SO_4$  and  $UO_2(SO_4)_2^{2-}$ , and in the neutral and alkaline regions, carbonate complexes  $UO_2CO_3$ ,  $UO_2(CO_3)_2^{2-}$ and  $UO_2(CO_3)_4^{4-}$ .

Coefficients of the Freundlich and Langmuir equations for isotherms of sorption of uranium (VI) compounds from mineralized waters

Sample	Langmuir			Freundlich		
	<i>a<sub>m</sub>,</i> mg/g	$K_L$ , dm <sup>3</sup> /mg	R <sup>2</sup>	<i>K<sub>F</sub>,</i> dm <sup>3</sup> /g	1/л	<i>H</i> <sup>2</sup>
MMT	0.42	0.039	0.976	0.06	2.52	0.941
Fh-MMT 0.01-1	0.28	0.0393	0.963	0.024	0.5374	0.968
Fh-MMT0.1-1	3.54	0.0389	0.971	0.362	0.4738	0.9897
Fh-MMT 0.5-1	9.89	0.0262	0.9386	0.396	0.7033	0.9801
Fh-MMT 1-1	10.13	0.0418	0.9642	0.392	0.7965	0.9915

Mineralized waters at the liquid waste storage facility for uranium ore processing contain cations of other metals. Therefore, the features of sorption of uranium from mineralized waters on iron oxide composites were studied under conditions of equimolar contents of uranium (VI) and cadmium (II), cobalt (II) cations, chromium (VI), manganese (II), arsenic (V). The distribution of various forms of these metals in the studied solutions (concentration of  $10^{-4}$  M in solution, mineralization of 5.2 g/l and pH of 7.2) are given in Table 4.

#### Table 4

Distribution of the forms of coexisting cations U(VI), Cd(II), Co(II), Cr(VI), Mn(II), As(V) in saline waters

Form	Content, % (for each Me)	Content, % (of the total metal content)
UO <sub>2</sub> CO <sub>3</sub>	2	0.3
$(UO_2)_2CO_3(OH)_3^-$	15	2.5
(UO <sub>2</sub> ) <sub>2</sub> (CO <sub>3</sub> ) <sub>2</sub> <sup>2-</sup>	45	7.5
$(UO_2)_2(CO_3)_3^{4-}$	43	7.2
$H_2AsO_4^-$	25	4.2
$HAsO_4^{2-}$	75	12.5
CdCO <sub>3</sub> (c)	98	16.3
CdSO <sub>4</sub>	2	0.3
CoSO4	78	13
Co <sup>2+</sup>	18	3
CoCO <sub>3</sub> (s)	4	0.7
$HCrO_{4}^{-}$	12	2
NaCrO <sub>4</sub>	21	3.5
Cr04 <sup>2-</sup>	67	11.2
MnCO <sub>3</sub> (c)	88	14.7
MnSO <sub>4</sub>	8	1.3
Mn <sup>2+</sup>	3	0.5
MnHCO <sub>3</sub> <sup>+</sup>	1	0.2

Experiments on the sorption extraction of uranium (VI) from mineralized waters in the presence of coexisting cations Cd(II), Co(II), Cr(VI), Mn(II), As(V) show that the presence of the latter in solution (in equimolar amounts in relation to uranium) does not significantly affect the sorption value. This allows not to take into account their influence on sorption processes in the approximate calculation of the corresponding technological processes.

# 7. SWOT analysis of research results

Table 3

*Strengths.* The main advantage of using iron oxide composites based on natural clay minerals to purify water from pollution by uranium compounds is their environmental friend-liness, low cost, accessibility and manufacturability. Similar sorption materials are obtained using complex synthesis schemes and expensive chemicals, which significantly increases their cost.

*Weaknesses.* When using reagents based on iron (III) salts with a high degree of purity

in the synthesis of bentonite/iron oxide composites, the cost of the synthesis product increases.

*Opportunities.* The use of bentonite/iron oxide composites for the extraction of uranium (VI) from complex aqueous systems, including solutions with high salinity and the presence of competing metals, is a promising area in environmental chemistry. The development of the technology of granulation of iron oxide composites will allow for the effective removal of sorption materials and the subsequent reliable disposal of waste water.

*Threats.* The presence on the world market of highly effective, but expensive sorption materials based on ion-exchange resins, activated carbon, synthetic metal oxides creates a fairly strong competitive environment.

### 8. Conclusions

1. By treating the surface of montmorillonite with ferric compounds, bentonite/iron oxide composites are obtained. The application of the ferrihydrite layer on the surface of montmorillonite led to a change in the parameters of the porous structure of the obtained material, namely, an increase in the specific surface from 89 m<sup>2</sup>/g to 250 m<sup>2</sup>/g and an increase in the average pore size to 1.72 nm. The X-ray amorphous nature of the obtained bentonite/iron oxide composites, a change in their electrokinetic properties and an increase in dispersion due to modification indicate the presence of iron oxide-hydroxide (III) on the surface of montmorillonite.

2. The features of sorption removal of uranium compounds from mineralized waters using the obtained bentonite/iron oxide composites are studied. It is shown that as a result of surface modification of montmorillonite by ferric compounds, the sorption capacity of materials for uranium compounds increases with an increase in the iron content on the surface: from 0.42 mg/g for montmorillonite to 10.13 mg/g for modified montmorillonite. It is found that the presence of competitive metals (As, Mn, Co, Cd, Cr) in mineralized waters in equimolar amounts does not lead to a significant change in the values of uranium adsorption on bentonite/iron oxide composites.

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