

## ABSTRACT AND REFERENCES

## ECOLOGY

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**CONSTRUCTION OF A GENERALIZED MODEL OF THE HARMFUL SUBSTANCES BIOCHEMICAL DESTRUCTION PROCESS KINETICS UNDER CONDITIONS OF SUBSTRATE INHIBITION USING THE METHODS OF SIMULATION MODELING (p. 6–16)**

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For the purpose of obtaining the complete range of solutions for substrate inhibition of varying intensity, the mechanism of enzyme kinetics in a biocell was modeled by a multi-channel queuing system. A full range of solutions is required to make a well-grounded choice of a unified generalizing formula. The process of biodegradation with substrate inhibition was described mathematically using the method of dynamics of averages. For specific destruction rate, a full range of solutions  $V_n$  of the system from minimum  $n=2$  to limiting  $n \rightarrow \infty$  order was found. It was established that the parameters of the curve shape for the solution with minimum inhibition intensity  $V_2$  substantially stand out from the general series of the spectrum formulas. The value of the coordinate of function maximum ( $n=2$ )  $V_2$  is by 1.42 times higher than that of dependence ( $n=3$ )  $V_3$ .

In the numerical experiment, the physical test was simulated by description with the help of the method of the least squares of the data, assigned by the calculation from the formulas of different structures, bearing in mind a sporadic random error. The series of numerical experiments demonstrated the capability of the formula of limiting order formula  $V_e$  to describe the dependences of the whole spectrum of solutions. During describing the intermediate ratio  $V_3$  with the help of formulas  $V_2$  and  $V_e$ , the benefit is the possible range of changing the concentrations, which is by 1.5–2 times larger at the same relative error for dependence  $V_e$ . For critical minimal order, an average relative error is sure not to exceed five percent. An increase

in random error always result in statistical equality, in accuracy of describing by formulas of minimal  $V_2$  and limiting orders  $V_e$  of the data, assigned by calculation of second-order dependences. Statistical equality is achieved at the ratio of a random error to the initial error equal to  $\geq 2.4$ .

Collectively, the importance of the results of numerical modeling of a physical experiment involves proving the possibility of using the formula of limiting order  $V_e$  as unified when describing the biodegradation processes with different mechanisms of substrate inhibition. This conclusion is proved by the adequate ( $R^2=0.9396-0.9953$ ) description with the help of the dependence of limiting order of experimental data on five harmful substances with varying inhibition degrees. A large amount of calculation allowed achieving a definite result – we obtained the unified formula that makes it possible to proceed to scientifically grounded design calculations for bio-treatment plants.

**Keywords:** biodegradation, substrate inhibition, queuing system, numerical experiment, unified formula.

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**USE OF FLY ASH FOR CONDITIONING THE EXCESS ACTIVATED SLUDGE DURING DELIQUFEACTION AT CHAMBER-MEMBRANE FILTER PRESSES (p. 17–23)**

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Results of experimental studies of deliqufeaction of excess activated sludge from municipal wastewater treatment facilities in chamber-membrane filter presses were presented. To condition the sludge, fly ash from thermal power plants was added as a mineral additive. Experimental studies have shown high efficiency of deliqufeaction of the excess activated sludge with addition of fly ash. Increase in the dose of fly ash has led to an overall increase in filtration capacity and a decrease in moisture content in the filter cake. It was found that in the case of adding fly ash in an amount of 2 wt. % of the initial sludge, deliqufeaction efficiency did not increase significantly. In this case, filtering time was reduced only by 15 % and specific capacity increased by 12 %. In the case of increasing the proportion of fly ash to 6 wt. % of initial sludge, a more intensive acceleration of the process was observed. Filtering duration was reduced from 100 to 10 min, specific capacity increased from 87 to 400 l/m<sup>2</sup>·hr.

Experimental studies have shown that addition of fly ash to sediments of municipal wastewater treatment facilities as a mineral component provides the possibility of deliqufeaction of the suspensions obtained using a chamber-membrane filter press. With optimal doses of 4–5 wt. % of the mass of initial sludge, filter capacity is expected to be 350–400 l/m<sup>2</sup>·hr. The resulting filter cake had moisture content of about 60 %, a dense, dry structure making it possible to transport it in bulk.

**Keywords:** chamber-membrane filter press, conditioning, fly ash, deliqufeaction, filtering duration, activated sludge.

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## DESIGN OF FIRE-RESISTANT HEAT- AND SOUNDPROOFING WOOD WOOL PANELS (p. 24–31)

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The conducted research revealed the possibility to manufacture heat- and soundproofing materials for the arrangement of buildings. Wood fibers, which are produced in the form of flat panels, are the raw materials for their production. The mechanisms for the process of heat- and soundproofing during energy transfer through the material, which enables influencing this process, were established. It was proved that they are related to the porosity of the material. Thus, at a decrease in volume weight of the material, thermal conductivity and sound transmission are reduced, and vice versa. In addition, heat- and soundproofing building materials from wood should meet the following requirements: to have stable thermal insulation and acoustic indicators within the whole operation period and to be fire resistant, not to give off hazardous substances into the environment. Experimental research proved that the material based on wood wool and inorganic binder at the ratio of 1:1 belongs to combustible materials, because there was its smoldering during the temperature exposure. Thus, under thermal exposure for 90 seconds, the sample caught fire, the flame propagated around the first three zones within 41 s. At the same time, an increase in the amount of the binder on inorganic base and application of organic-mineral binder does not lead to the ignition of material, the maximum temperature of flue gases made up around 120 °C and flammability index amounted to 0. This became possible due to the decomposition of fire retardants under the influence of temperature with emitting non-combustible gases, inhibiting the processes of material oxidation and significantly increasing the formation of the heat protective layer of coke on the surface of the material. This leads to inhibition of heat transfer of high-temperature flame to the material. This made it possible to determine the conditions for fire-resistance of the material through the formation of a thermal conductivity barrier. This makes it possible to argue about the relevance of the detected mechanism of formation of properties of the material based on wood wool and inorganic or organic-mineral binder, as well as practical attractiveness of the proposed technological solutions. The latter, in particular, relate to determining the amount of the binder component (the ratio of wood wool to the binder is not less than 1:2), because in small quantities (ratio 1:1), the burning process occurs. Thus, there are the grounds to argue about the possibility of directional regulation of the processes of formation of heat- and soundproofing wood materials through the use of wood wool and the binder. In this case, it was proposed to use the inorganic and organic-mineral coatings as a binder, which can form a fireproofing film at the surface of the material.

**Keywords:** heat- and soundproofing materials, wood wool, thermal conductivity, soundproofing, inorganic and organic-mineral binder.

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**DEVELOPMENT OF A METHOD FOR OPTIMIZATION CALCULATION OF A GROUP OF SOUND-INSULATING PANELS FOR AIRBORN NOISE PROTECTION (p. 32–38)**

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Various designs and procedures for calculating soundproof panels for protecting premises against airborne noise were considered. These procedures make it possible to calculate single-layer, two-layer and three-layer panels. Single-layer panels may consist of homogeneous solid and thin materials. Two-layer panels may consist of two thin layers of different thickness and an air gap. Three-layer panels can be made of two thin layers of different thickness and a sound-absorbing material between them. These procedures enable calculation and optimization of individual structures of sound-proofing panels independently of each other. The problem of simultaneous penetration of noise from one source into several adjacent rooms was considered. When using the procedures considered in references, maximum effect is unattainable. In this regard, a method of optimization calculation of a group of sound-proofing panels aimed at achievement of the most advantageous value of the objective function was proposed.

The method is based on a random search resting on random distribution of typical structures and procured materials among panels. Choice of the best result is made proceeding from a result of checking fulfillment of limiting conditions.

The following options of the objective function were proposed: the excessive noise load, the total index of noise reduction in rooms, the total cost of sound-proofing panels and the number of panels made. Recommendations were given on the choice of the objective function option taking into account concrete production conditions.

The result of optimization consists in the choice of design of the panel for each room and distribution of available materials among them. Formulation of the optimization problem with various options of the objective function and limitations has been considered. Efficiency of using this method was confirmed by almost 24 % lower cost of panels compared to the separate panel designing using conventional methods.

**Keywords:** noise, multilayer panels, sound insulation, optimization calculation, calculation algorithm, objective function.

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## ASSESSMENT AND PREVENTION OF THE PROPAGATION OF CARBON MONOXIDE OVER A WORKING AREA AT ARC WELDING (p. 38–49)

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This paper reports a study of air environment at industrial premises where welding processes take place, with special attention paid to the formation of carbon monoxide (oxide) (CO) in the working environment in the process of manual arc welding. We have given the classification of basic harmful substances generated during welding and related processes in terms of the character of negative influence on the body of a welder. A mathematical model of the dynamics of change in the concentration of carbon monoxide in the air of a working area has been constructed, based on the amount of a harmful substance ( $m$ ) in the air at premises at a time point, the intensity of its release into air, and the air exchange rate. A given mathematical model includes the propagation of carbon monoxide in the air, considering the air exchange between the overall volume of a premise and the local volumes of working zones.

There are not enough studies into the formation of carbon monoxide during welding processes, which is why examining this process is a priority.

Our experimental study has confirmed that the concentration of carbon monoxide outside the local volumes of local ventilation devices, that is in the air of working zones, remains constant (to 0.01 mg/m<sup>3</sup>) and does not exceed MPC (20 mg/m<sup>3</sup>). A failure or the absence of general ventilation leads to a rapid increase in the concentration of carbon monoxide (CO) in line with an exponential dependence (from 150 to 200 mg/m<sup>3</sup> over 0.5–0.6 hours) within a small closed workspace (1 m<sup>3</sup>), and can quickly spread throughout the entire premise.

However, a failure or the absence of general ventilation leads to a rapid increase in the concentration of carbon monoxide (CO) in line with an exponential dependence. This indicates that general ventilation is important, but it does not warrant safety for welders and other workers from gas poisoning. Therefore, the use of local ventilation must be ensured, as well as respiratory protection for all present when conducting welding processes. The derived mathematical models make it possible to assess risks during welders' operations, to take into consideration CO emissions when calculating ventilation systems in working areas, to adjust the system that manages risks and labor safety.

**Keywords:** arc welding, carbon monoxide, harmful emissions, workspace, gas poisoning.

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**DEVELOPMENT OF A HIGHLY EFFICIENT COMBINED APPARATUS (A COMBINATION OF VORTEX CHAMBERS WITH A BIN) FOR DRY DEDUSTING OF GASES (p. 49–55)**

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The use of dust collectors of a new type which combine the operation principle of centrifugal and louver-vortex apparatuses was considered. The use of a heterogeneous reactor for gas-solid systems with two streams in a cyclone, a direct-flow cyclone with a chamber of preliminary collision of gas-dust flows, as well as improved designs of vortex chambers was considered.

A combined dust collector was presented in a form of the Rankine vortex tube in combination with a bin in which louver-vortex devices are installed. The combined deduster under study provides an organized supply of a gas-dispersed system at adjustable hydrodynamic conditions to louver-vortex devices used as the dedusting apparatus. It was assumed that the processes of coagulation of particles under appropriate hydrodynamic conditions as well as partial destruction of harmful gas impurities in a continuous phase will take place in the vortex tube. Thus, development of a substantiated physical model (of a design) of a combined dust collector for specified initial conditions and operability of the design were considered on the basis of theoretical and experimental provisions.

It has been established that creation of hydrodynamic conditions in centrifugal devices and pipelines is the most promising direction of increasing the degree of dedusting of a gas-dispersed flow. These conditions must ensure supply of the gas-dispersed system to the centrifugal apparatus to ensure agglomeration of fine particles.

Design of a dedusting apparatus in which intense collision of dust particles in a special chamber and their agglomeration and subsequent separation supposed to proceed in a chamber which is actually a cyclone is an expedient and effective solution. It provides the degree of purification of the gas and dust flow at a level of 98–99 % regardless of particle size.

**Keywords:** vortex tube, hydrodynamic conditions, cleaning efficiency, dust separation, combined apparatus, dust flow.

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